

## CLAIM AMENDMENTS

1. (currently amended) In a process for the continuous production of polyesters (PES) by esterification/transesterification of dicarboxylic acids, preferably ~~terephthalic acid~~, or esters of the dicarboxylic acids with diols, preferably ~~ethylene glycol (EG)~~, in at least one reaction stage, prepolycondensation of the esterification/transesterification product under [[a]] vacuum by means of a reaction stage consisting of a vertical reactor, and polycondensation of the prepolycondensation product in at least one polycondensation stage, ~~characterized in that~~ the improvement comprising the steps of:

flowing the esterification/transesterification product flowing into the vertical reactor [[, ]] and maintaining in the vertical reactor ~~which there exists~~ a pressure of 10 to 40 % of the diol equilibrium pressure of the prepolycondensation product leaving the reactor and a process temperature of 268 to 274°C [[,]]; and

successively traverses passing the esterification/transesterification product in a free movement without stirring under limited heating first through at least one first reaction zone formed of an annular channel, then ~~is~~ introduced into the radially outer or the radially inner ring duct of at least one second reaction zone formed of an annular channel divided into a plurality of concentric ring ducts [[, is]] where

the product passes successively passed through the ring ducts to the outlet and then into a stirred third reaction zone located at the bottom of the reactor.

2. (original) The process as claimed in claim 1, characterized in that the total pressure of the reaction product at the bottom the channels of the first and second reaction zones is smaller than the local diol equilibrium pressure of the polycondensation product.

3. (currently amended) The process as claimed in claim 1, characterized in that the total pressure of the reaction product at the bottom of the channels of the first and second reaction zones is 5 to 80 % , ~~preferably 10 to 70 %~~ of the local diol equilibrium pressure of the polycondensation product.

4. (previously presented) The process as claimed in claim 1, characterized in that the vapors formed in the three reaction zones are jointly withdrawn from the reactor.

5. (previously presented) The process as claimed in claim 1, characterized in that the vapors of the first reaction zone are supplied to a separator for the entrained product droplets, before they are combined with the vapors of the two other reaction stages.

6. (previously presented) The process as claimed in claim 1, characterized in that the reaction product is concurrently passed in parallel through adjacent ring ducts of the second reaction zone.

7. (previously presented) The process as claimed in claim 1, characterized in that the reaction product is countercurrently passed in parallel through the ring ducts of the second reaction zone.

8. (previously presented) The process as claimed in claim 1, characterized in that the product level of the stirred third reaction zone is controlled.

9. (previously presented) The process as claimed in claim 1, characterized in that the product level in the channel of the first reaction zone and in the ring ducts of the second reaction zone is kept constant.

10. (previously presented) The process as claimed in claim 1, characterized in that the product level in the ring ducts of the second reaction zone is lower than in the channel of the first reaction zone by a factor of 2 to 3.5.

11. (previously presented) An apparatus for performing the process as claimed in claim 1, characterized by a heating tube

register arranged in the channel of the first reaction zone and extending in flow direction, whose tubes are retained in chambering sheets mounted transverse to the flow direction.

12. (original) The apparatus as claimed in claim 11, characterized by a closed vapor collecting space mounted above the channel of the first reaction zone, whose outlet opening is connected with a separator for the entrained product droplets.

13. (previously presented) The apparatus as claimed in claims 10, characterized by an overflow baffle plate or overflow tube arranged at the end of the channel of the first reaction zone.

14. (previously presented) The apparatus as claimed in claim 10, characterized by an overflow baffle plate or overflow tube arranged at the end of each ring duct of the second reaction zone.

15. (previously presented) The apparatus as claimed in claim 10, characterized in that an underflow baffle plate or a riser is provided upstream of each overflow baffle plate or overflow tube.

16. (previously presented) The apparatus as claimed in claim 10, characterized by a gooseneck outlet with drainage bypass and vent tube each arranged at the deepest point of the bottom at

the end of the channel of the first reaction zone or at the end of the last ring duct of the second reaction zone.

17. (previously presented) The apparatus as claimed claim 10, characterized by a drainage opening each located at the deepest point of the bottom at the end of the channel of the first reaction zone or at the end of each ring duct of the second reaction zone.

18. (previously presented) The apparatus as claimed in claim 10, characterized in that guide plates are arranged in the ring ducts of the second reaction zone.

19. (currently amended) The apparatus as claimed in claim 10, characterized in that the bottom of the channel of the first and/or second, reaction zone is inclined at an angle of 0.5 to 6 , ~~preferably 1 to 4~~ with respect to the horizontal plane.

20. (previously presented) The apparatus as claimed in claim 10, characterized in that the stirrer for the third reaction zone consists of a ground-running impeller, finger, frame or drum stirrer, each with a vertical drive axle.

21. (previously presented) The apparatus as claimed in claim 10, characterized in that the stirrer for the third reaction

zone includes a rotary-disk stirrer or a cage stirrer, each with a horizontal drive axle.

22. (original) The apparatus as claimed in claim 21, characterized in that the rotary-disk stirrer is equipped with perforated, ring or solid disks.

23. (original) The apparatus as claimed in claim 22, characterized in that in a rotary-disk cascade the inlet for the reaction product is half mounted at each of the axial ends, and the common outlet is mounted in the middle.

24. (original) The apparatus as claimed in claim 22, characterized in that in the rotary-disk cascade with perforated disks the inlet for the reaction product is mounted at the one end and the outlet is mounted at the opposite end.

25. (previously presented) The apparatus as claimed in claim 10, characterized by one stationary partial stream drainage each mounted at the bottom at the ends of the channels and of the ring ducts.